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2 **Intercalation and Retention of Carbon Dioxide in a Smectite Clay promoted by**
3 **Interlayer Cations**

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14 **Abstract: A good material for CO₂ sequestration should possess some specific**
15 **properties: (i) a large effective surface area with good adsorption capacity,**
16 **(ii) selectivity for CO₂, (iii) regeneration capacity with minimum energy**
17 **input, allowing reutilization of the material for CO₂ adsorption, and (iv) low**
18 **cost and high environmental friendliness. Smectite clays are layered**
19 **nanoporous materials that may be good candidates in this context. Here we**
20 **report experiments which show that gaseous CO₂ intercalates into the**
21 **interlayer nano-space of smectite clay (synthetic fluorohectorite) at**
22 **conditions close to ambient. The rate of intercalation, as well as the**
23 **retention ability, of CO₂ and it was found to be strongly dependent on the**
24 **type of the interlayer cation, which in the present case is Li⁺, Na⁺ or Ni²⁺.**
25 **Interestingly we observe that the smectite Li-fluorohectorite is able to retain**
26 **CO₂ up to a temperature of 35 °C at ambient pressure, and that the captured**
27 **CO₂ can be released by heating above this temperature. Our estimations**
28 **indicate that smectite clays, even with the standard cations analyzed here,**
29 **capture CO₂ per volume comparable to other materials studied in this**
30 **context.**

31 Interactions between CO₂ and clay minerals have attracted interest in the
32 scientific community in recent years, partly because geological structures are
33 being investigated as storage sites for anthropogenic CO₂. The cap-rock
34 formations which act as flow barriers and seals in this context are known to
35 contain high proportions of clay minerals¹, and the long-term integrity of these
36 formations is a prerequisite for avoiding CO₂ losses to the atmosphere^{2,3}.
37 However, the physical parameters affecting the interactions between CO₂ and
38 clay minerals under reservoir conditions are still not well understood⁴.

39 Clay minerals are materials based on two-dimensional stacks of inorganic layers⁵.
40 In some clay minerals (smectites), non-equivalent substitutions of atoms
41 generate a negative charge on each layer surface which is balanced by
42 exchangeable interlayer cations. These cations are responsible for the differences
43 in the physico-chemical behavior of smectites such as water adsorption and
44 retention, plasticity, swelling etc^{6,7}. Smectite clay mineral particles typically
45 consist of up to several hundred layers. Smectites have the ability to intercalate
46 additional molecules into the interlayer space, thereby changing the repetition
47 distance along the layer normal, a process which is known as swelling^{8,9}.
48 Intercalation of water can also occur, since H₂O is a polar molecule, and has
49 been extensively studied with a wide range of techniques, such as neutron^{8,10,11}
50 and X-ray scattering^{9,12,13}, NMR spectroscopy¹⁴⁻¹⁶ tracer experiments¹⁷ or
51 numerical modeling^{14,18}.

52 Experiments¹⁹⁻²⁸ and simulations^{18,29-32} have also shown that CO₂ intercalates in
53 some smectite clays, both in supercritical, and in gaseous/liquid form. We have
54 recently demonstrated that CO₂ is able to intercalate in Na-fluorohectorite (NaFh)
55 smectite clay mineral at conditions close to ambient (-20 °C, 5 bar)²². These are
56 not the typical conditions found in geological storage sites, but the conditions are
57 relevant if clays are considered as a potential material for the capture or
58 sequestration of CO₂, and also it is of great interest to study CO₂ capture and
59 retention under these conditions for the purpose of understanding the underlying
60 molecular mechanisms. Several porous materials are currently being assessed for
61 the purpose of CO₂ capture and retention³³⁻³⁵. In this context, clay-containing
62 materials could have a distinct advantage in that they are both cheap and
63 ubiquitous³¹, and also because they generally provide a very large accessible
64 effective surface area that arises from nanolayered stacked structures embedded
65 in a mesoporous powder matrix.

66 Fluorohectorites (Fh) are synthetic smectites which have been used as a
67 representative and clean model system of natural smectite clays³⁶. Synthetic
68 clays have the advantage that they possess a more homogeneous charge
69 distribution, and also contain significantly fewer impurities (e.g. carbonates,
70 (hydr)oxides, silica, and organic matter) than their natural counterparts³⁷.

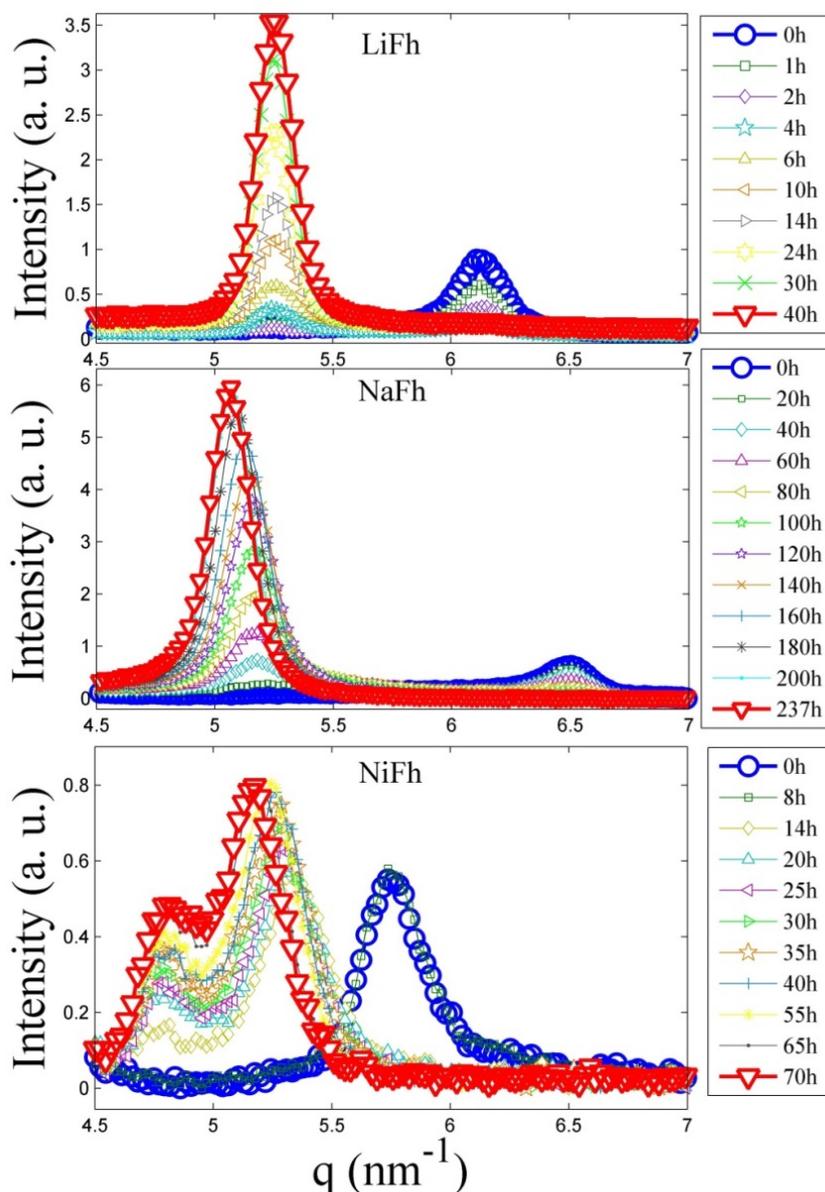
71 In the present work we studied the intercalation of CO₂ in Li-fluorohectorite
72 (LiFh), Na-fluorohectorite (NaFh) and Ni-fluorohectorite (NiFh). The only
73 differences between these samples are the interlayer charge compensating
74 cations used. Intercalation experiments under different temperature and pressure
75 conditions were conducted. In order to investigate the potential of fluorohectorite
76 clays for CO₂ storage and capture, we also quantified the CO₂ adsorption (wt%).

77 **Results**

78 **A. CO₂ Intercalation**

79 The layered nature of smectite clays gives rise to well-defined (00l) diffraction
80 peaks, and the angular position of these peaks is a direct measure of the interlayer
81 repetition distance (the d-spacing). Figure 1 displays how the intensity of the (001)
82 diffraction peak grows with time as the samples are exposed to CO₂ at -20 °C and 20
83 bar. Intercalation of CO₂ in the interlayer space manifests itself as the growth of an
84 intercalation peak at a lower scattering angle than the peak of dry, non-intercalated
85 clay. As the intercalation progresses, the intensity of the CO₂-intercalation peaks
86 increase whereas the scattering from non-intercalated part of the sample decreases
87 and eventually vanishes. LiFh and NaFh show similar intercalation behaviors and the
88 (001) peaks develop at q-values corresponding to d-spacings of 1.196 nm
89 ($q = 5.25 \text{ nm}^{-1}$) and 1.240 nm ($q = 5.06 \text{ nm}^{-1}$), for LiFh and NaFh respectively. This
90 corresponds to a monolayer of intercalated CO₂. For the NiFh sample we observe a
91 similar intercalation state with d-spacing of 1.219 nm ($q = 5.15 \text{ nm}^{-1}$) and in addition
92 the development of another state with a larger d-spacing of 1.311 nm

93 ($q = 4.79 \text{ nm}^{-1}$). To our knowledge, this is the first time such a complex CO_2
 94 intercalation state has been observed in clay mineral.

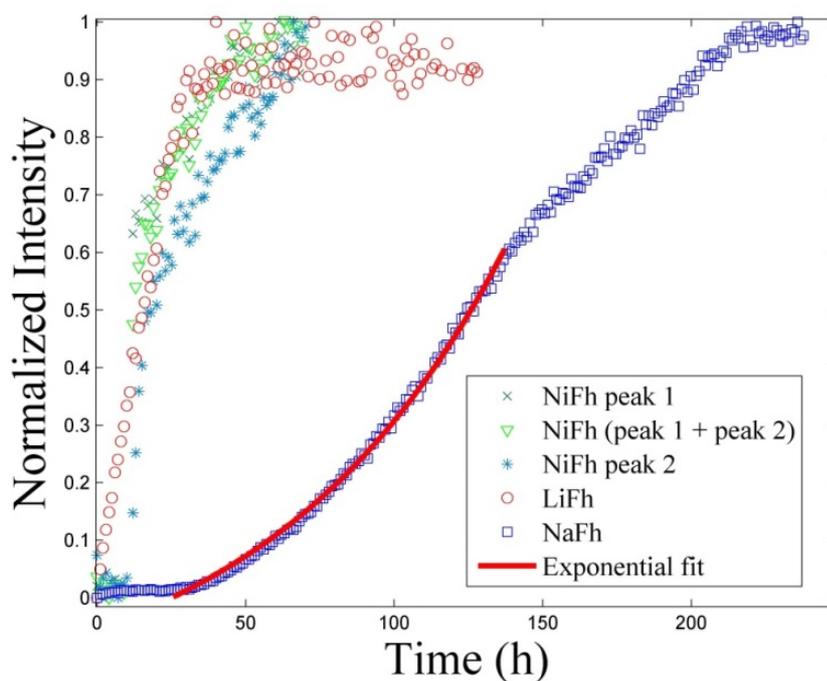


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96 Figure 1: The scattering intensity (arb. units) over a range of q -values at different
 97 times (hours), for LiFh, NaFh and NiFh, respectively. In all cases the adsorption
 98 conditions were $-20 \text{ }^\circ\text{C}$ and 20 bar. The red line (∇) shows the time at saturation.
 99 Experiment performed at NTNU.

100 Figure 2 shows the comparison of (001) peak intensity vs. time for LiFh, NaFh
 101 and NiFh. In this figure the NiFh (001) peak intensities are the one at higher
 102 $q \approx 5.2 \text{ nm}^{-1}$, the one at lower $q \approx 4.8 \text{ nm}^{-1}$ and the sum of them, as shown in

103 figure 1. We observe that the intercalation rate is significantly higher for NiFh and
104 LiFh than for NaFh. This is similar to the case of water intercalation, where cations
105 have been found to determine the stable states at varying relative humidity^{18,38-41} as
106 well as the way that clay minerals exfoliate in aqueous dispersion^{7,42}. Fripiat et al.²⁷
107 suggested that the access of CO₂ molecules to the interlayer space of montmorillonite
108 clay is dependent on the size of the interlayer cation. On the other hand, Giesting et
109 al.²³ studied CO₂-intercalation behavior of K-and Ca-montmorillonite, and also
110 performed repeated measurements under the same conditions, but reported no
111 strong dependence of dynamics on the cations. The dynamics of the CO₂ intercalation
112 can also be followed by observing the disappearance of the scattering intensity of the
113 dehydrated peak, shown in figure S1 in supporting information, which represents the
114 d-spacing in the portion of the sample with no water or CO₂ intercalated.



115

116 Figure 2: Intensity of the intercalation peak, normalized to the maximum intercalation
117 intensity, as a function of time for different cations at 20 bar and -20 °C. The NiFh
118 diffractogram has two contributions: Peak 1 is the peak with the maximum intensity
119 at highest $q \approx 5.2 \text{ nm}^{-1}$ while peak 2 is the peak with the lowest $q \approx 4.8 \text{ nm}^{-1}$.

120 A general equation for describing sorption kinetics is⁴³:

$$121 \quad \frac{dn}{dt} = n_0 \frac{1}{\tau} f\left(\frac{n}{n_0}\right) \quad (1)$$

122 where n is the amount of adsorbed molecules on a surface and $\frac{1}{\tau}$ is a rate constant

123 that depends on temperature and pressure. The equation for the function $f\left(\frac{n}{n_0}\right)$

124 depends on the type of adsorption mechanism. For a first order adsorption process,

125 i.e. a process where the adsorbed molecules statistically occupies a single adsorption

126 site⁴⁴, $f\left(\frac{n}{n_0}\right) = 1 - \frac{n}{n_0}$. In the present case, $\frac{n}{n_0}$ is equal to normalized X-ray intensity

127 (NI), where normalization is performed with respect to the intensity observed at the

128 longest times, where the adsorption capacity of the material is reached. By

129 integrating equation (1), we obtain

$$130 \quad NI = 1 - \exp\left(-\frac{t}{\tau}\right) \quad (2)$$

131 which is an exponential growth function towards saturation at 1. Applying the

132 natural logarithm, we have a linear equation with the slope proportional to the rate

133 constant $\frac{1}{\tau}$:

$$134 \quad -\ln(1 - NI) = \frac{t}{\tau} \quad (3)$$

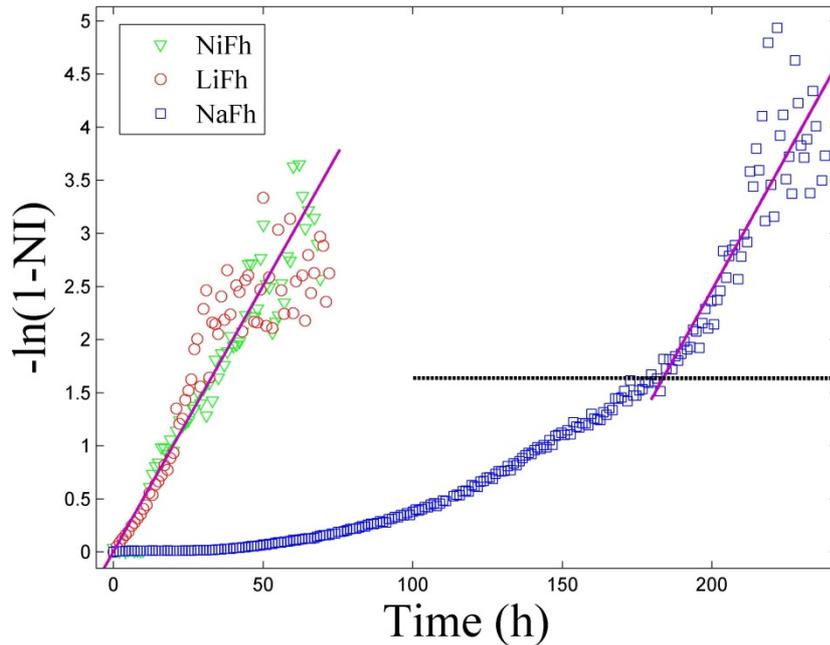
135 The results of plotting the observed normalized intensity in this manner are

136 shown in figure 3. It is evident that equation (3) describes the data for NiFh and LiFh

137 reasonably well, before the full adsorption capacity is reached, i.e. before all the sites

138 have been occupied. However, for NaFh we observe deviation for $-\ln(1 - NI) < 1.6$,

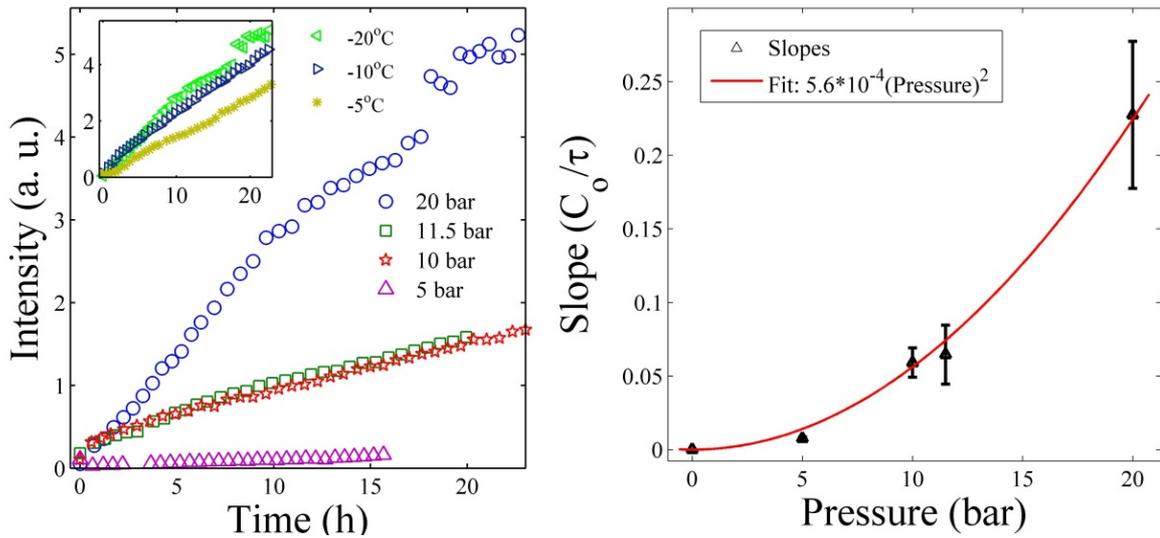
139 which we relate to the Na^+ ion providing a stronger layer adherence than the other
 140 two ions investigated here, and thus the swelling is more difficult to achieve for the
 141 case of Na^+ , since the clay layers are closer together in the dehydrated state of NaFh,
 142 as shown in figure 1. The difference Δq -spacing between the dehydrated and the CO_2
 143 intercalated peak is almost twice for NaFh compared to LiFh and NiFh (figure 1). The
 144 dotted horizontal line represents the threshold between two regimes for the case of
 145 NaFh: particle swelling plus intercalation of CO_2 (below the line) and intercalation of
 146 CO_2 into the swollen interlayer of the clay mineral (above the line). A single
 147 exponential growth function $NI = A \exp\left(\frac{t}{\tau_1}\right)$ (shown in figure 2), with $\tau_1 \approx 88$, related
 148 to the clay swelling, describes well the data in the initial phase for NaFh, i.e. for
 149 $-\ln(1-NI) < 1.6$ in figure 3.



150
 151 Figure 3: The linearized intensity as function of time. The horizontal dotted line
 152 represents the threshold between two regimes for NaFh: Clay swelling accompanied
 153 by some intercalation of CO_2 (below the horizontal line), which is described by the
 154 exponential function $NI = A \exp\left(\frac{t}{\tau_1}\right)$, and intercalation of CO_2 into the swollen
 155 interlayer of the clay mineral (above the horizontal line) described by equations (2)
 156 and (3). The initial swelling part of the dynamics is much faster for NiFh and LiFh as
 157 compared to NaFh, which is also confirmed in figure S1 in the supporting information.

158 After the swelling process is finished, which means that the clay does not
 159 expand significantly anymore, the intercalation process is cation independent since
 160 the slopes of the curves shown in figure 3 are the same for all samples, i.e.

161 $\frac{1}{\tau} = 0.05 \pm 0.005 \text{ hours}^{-1}$. This corresponds to a time constant τ of approx. 20 hours.



162

163 Figure 4: Left panel: The intensity of the (001) CO₂ intercalation peak in LiFh as a
 164 function of time for different pressures (at constant temperature of -20 °C). The
 165 intercalation rate increases with the pressure. Right panel: The quadratic dependence
 166 of the linear fit slopes C_0/τ on CO₂ pressure. Experiment performed at Maxlab.

167 The dependence of the intercalation intensity at various pressures is shown in
 168 figure 4 for LiFh. The results show that the intercalation rate increases with pressure
 169 and this observation is in agreement with a previous study of NaFh²². We also
 170 measured intercalation at various temperatures (at a constant pressure of 20 bar) in
 171 the limited temperature range -5, -10 and -20 °C and the data suggests (inset of
 172 figure 4) faster adsorption at lower temperature.

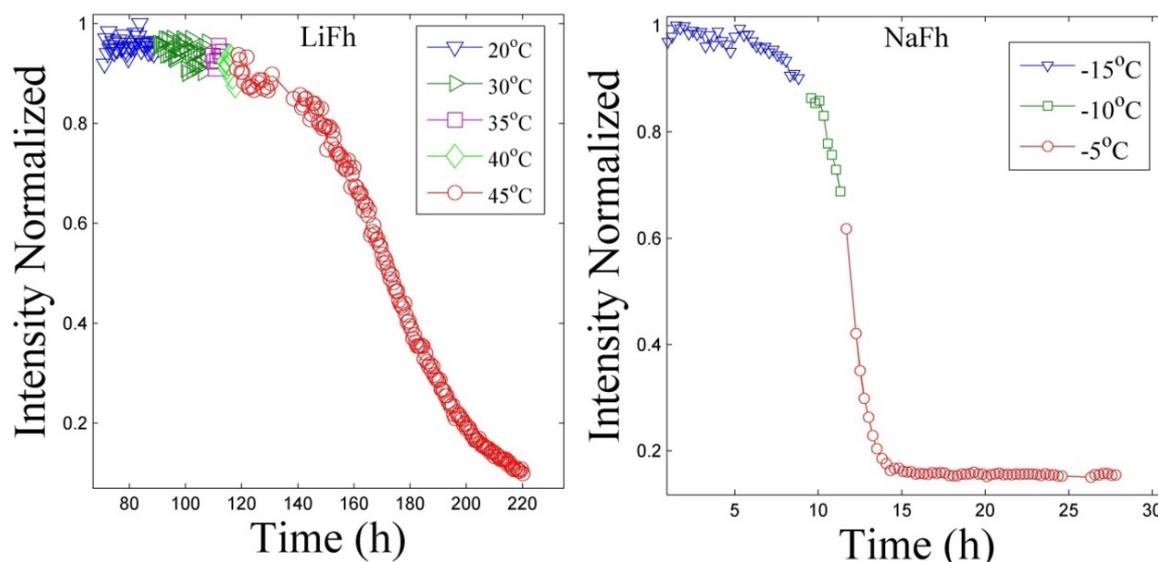
173 The intensity of the CO₂ intercalation peak follows a linear behavior for small
 174 times, in agreement with equation (2), which for small times $t \ll \tau$ becomes $NI \approx \frac{t}{\tau}$
 175 . In figure 4 we have not normalized the measured intensities to their saturation at
 176 long times, because we did not follow the experiments until saturation, thus the

177 slopes (S) of the straight lines at short times in figure 4: $S \approx \frac{C_o}{\tau}$ where C_o is a
178 constant. If we assume that the adsorption dynamics after swelling is governed by an
179 average Arrhenius like trapping time, $\tau = \tau_o e^{-\frac{E}{k_B T}}$, where, $\frac{1}{\tau_o}$ is an average attempt
180 frequency, E is an average energy barrier, k_B is Boltzmann constant and T is the
181 absolute temperature. Further we can assume that the attempt frequency $\frac{1}{\tau_o}$
182 increases with pressure, P , i.e. the higher the pressure, the more attempts are made
183 by the CO_2 molecules to cross the adsorption trapping energy barrier E . In right
184 panel of figure 4, we have tested this assumption and fitted an empiric parabolic
185 function to the pressure dependence of $\frac{1}{\tau_o}$. Our temperature measurements are in a
186 such limited range in absolute temperature that they do not allow us to test Arrhenius
187 trapping time assumption, but the desorption data for LiFh (shown below) indicates
188 that the sorption trapping barrier is on the order of magnitude of $\frac{E}{k_B} \approx 300K$. This
189 gives $\tau \approx \tau_o \frac{6 \times 10^{-4}}{P^2} e^{-\frac{300}{T}}$ where P is in units of bar and T in units of absolute
190 temperature (K). From figure 3 we estimated $\tau \approx 20$ hours for P and T equal to 20
191 bar and 253 K respectively. This enables us to estimate $\tau_o \approx 5 \cdot 10^7$ hours, and thus
192 the adsorption time would be $\tau \approx 14$ min for P and T equal to 200 bar and 250 K
193 respectively, if we assume that trapping mechanism for liquid and gas CO_2 are the
194 same.

195 **B. CO_2 retention under ambient conditions**

196 After exposing the three types of clay mineral samples to CO_2 pressure for a
197 sufficiently long time, the CO_2 pressure was released and the cell was continuously
198 flushed with N_2 , since it is dry and does not intercalate in the clay minerals, at

199 atmospheric pressure, while increasing the temperature in steps of 5 °C. A plot of
200 peak intensity versus time at different increasing temperatures is shown in figure 5.

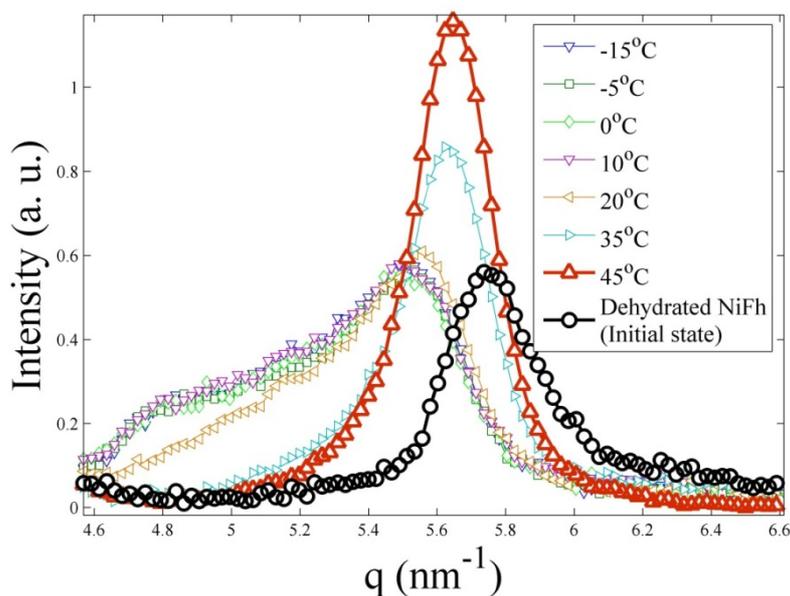


201

202 Figure 5: (001) peak intensity of LiFh (left) and NaFh (right) as a function of time for
203 increasing temperatures. Experiments performed at NTNU.

204 It has previously been concluded that the interlayer CO₂ may cause an irreversible
205 adsorption in clay, i.e. even if a clay sample is not exposed to the CO₂ gas, CO₂
206 molecules remain in the interlayer space^{45,46}. This means that once intercalated with
207 CO₂ the clay mineral will retain these molecules. However, a temperature change can
208 affect the CO₂ retention^{47,48} and this makes the process of intercalation and release
209 truly reversible. We found that at a certain threshold temperature, the intensity
210 decreases until the contribution to the scattered intensity from the clay mineral with
211 intercalated CO₂ is negligible. Simultaneously, the peak corresponding to the
212 dehydrated LiFh and NaFh reappears (data not shown). The threshold temperature, at
213 which the CO₂ is desorbed from the interlayer space of the clays, is highly dependent
214 on the type of interlayer cation used. For LiFh, this temperature is about 35 °C,
215 whereas for NaFh it is about -15 °C (figure 5). This is consistent with the difference in
216 size between the smaller Li⁺ cation versus the larger Na⁺ cation. Li⁺ has a more
217 concentrated charge distribution than Na⁺ and can thus polarize the CO₂ molecule

218 more, forming a stronger bond to it. In the case of NiFh the release, like the
219 intercalation, has more complex features, as shown in figure 6.



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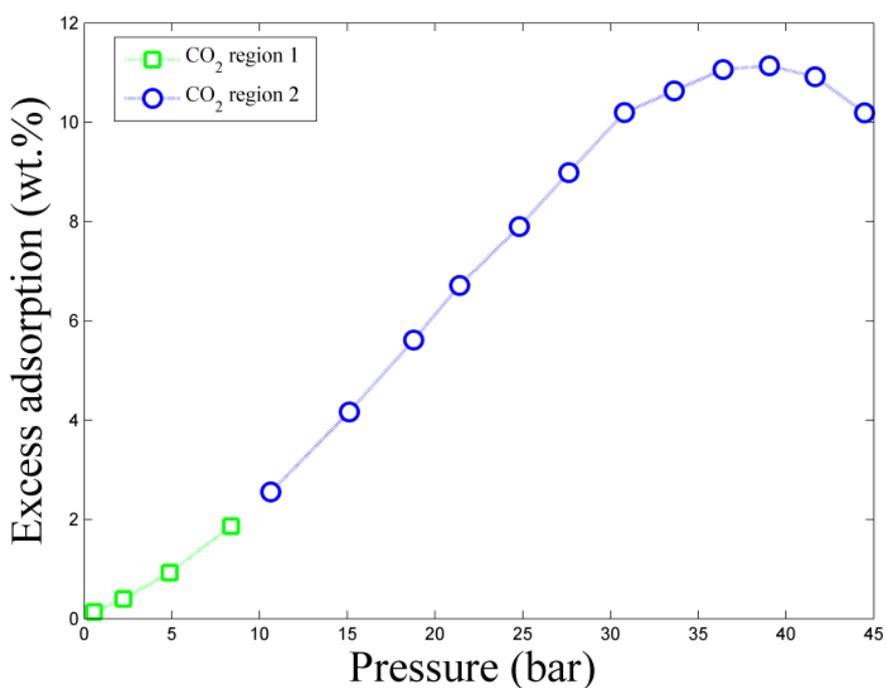
221 Figure 6: (001) peak intensity of NiFh as a function of the scattering vector q for
222 different temperatures in N_2 at atmospheric pressure. As a reference the initial
223 dehydrated peak of NiFh is included in the graph (circles, which is the same as the 0h
224 curve in figure 1). Experiments performed at NTNU.

225 Comparing NiFh spectrum in figure 1 with figure 6 one can see that upon
226 heating the second CO_2 peak merges with the first CO_2 peak for NiFh. With increasing
227 temperature, the intensity of the peak at lowest q value (about 4.8 nm^{-1}) decreases
228 and at $45\text{ }^\circ\text{C}$, it completely disappears while the highest q value peak shifts to higher
229 values and eventually contains all the (001) scattering. It appears that the final
230 intercalation state is different from the original dehydrated state. This could suggest
231 the formation of a complex CO_2-Ni^{2+} structure within the interlayer space of the NiFh
232 clay mineral, not present in the case of LiFh and NaFh.

233 C. Pressure composition Temperature Experiments

234 Figure 7 shows the excess CO_2 adsorption isotherm of LiFh, obtained with the
235 pCT-setup, described in the methods section. The excess adsorption is the amount of
236 material taken up by the sample. The adsorption measurements were performed at
237 room temperature and pressure range from 1 bar up to 45 bar. The initial part of the

238 isotherm (0 to ca. 9 bar) represents diffusion of CO₂ into the mesoporous network⁴⁹ of
239 the clay powder. Above approximately 9 bar it is likely that the swelling process of the
240 clay has nearly finished, and this will result in increased intercalation kinetics. With
241 further increase in CO₂ pressure, the excess of CO₂ is seen to rise up to around 11 wt.
242 % at a pressure of about 38 bar. At higher pressures, the apparent amount of
243 adsorbed CO₂ starts to decrease, likely due to the formation of an adsorbed layer with
244 higher density and comparable to the volume of the clay mineral, associated with
245 approach to the critical pressure for CO₂^{50,51}.



246
247

248 Figure 7: Excess CO₂ adsorption isotherm of Li-fluorohectorite at room temperature
249 and pressure range 0 to 45 bar. The region 1 (squares) describes diffusion of CO₂ into
250 the clay mineral powder mesoporous network, and subsequent intercalation within the
251 region 2 (circles). Experiment performed at IFE.

252

253 Discussion

254 The uptake of CO₂ per weight of clay mineral can be inferred if it is assumed
255 that the number of CO₂ molecules coordinating exchangeable cations is similar to the
256 number of H₂O molecules within the interlayer space for the corresponding H₂O-clay

257 system (at monohydrated state). This is approximately 2.4 molecules for each
258 interlayer cation^{16,15}. In case of LiFh and NaFh these would result in:

$$259 \quad \frac{m_{\text{CO}_2}}{m_{\text{NaFh}}} \approx \frac{m_{\text{CO}_2}}{m_{\text{LiFh}}} \approx 14\% \quad (3)$$

260 which is the same order of magnitude as measured by pCT (Figure 6), in this pressure
261 range. This gives an amount of 3.2 mmols of CO₂/g of LiFh, and makes the clay
262 minerals an interesting candidate for anthropogenic CO₂ storage. For other good CO₂
263 capturing materials this number vary from 6.00 mmol of CO₂/g, for e.g. metal organic
264 frameworks (MOFs)⁵², to 5.00 mmol of CO₂/g for Zeolites⁵³. Both numbers are higher
265 than the one we find for the clay mineral fluorohectorite. However, if we compare the
266 adsorbed mmol of CO₂ per volume of the material, rather than mmol of CO₂ per
267 adsorbent mass, considering that the densities of zeolites (~2.2 g/cm³) and MOFs
268 (~2.0 g/cm³) are lower than that of the clay minerals (~2.8 g/cm³). We find that a
269 clay mineral, even with the cations considered here, is able to capture nearly the
270 same mass of CO₂ per volume (0.23 ton of CO₂ per m³ of sample) as compared to the
271 "best" zeolites (0.29 ton of CO₂ per m³ of sample), or MOFs (0.32 ton of CO₂ per m³
272 of sample) in this context. These numbers were calculated assuming 60% of packing
273 density for all the materials. The commonly used benchmark Zeolite 13X captures
274 0.14 ton of CO₂ per m³ of sample.

275 **Methods**

276 X-ray diffraction measurements were primarily performed on an in-house
277 (NTNU, Trondheim) Bruker NanoSTAR X-ray scattering instrument, attached to a
278 Xenox stationary electron impact source with a copper anode, producing K α -radiation.
279 The scattered intensity was recorded by a two-dimensional multiwire grid Xe gas
280 detector (HI-STAR, Bruker). The beam diameter of the setup is 400 μm and the
281 detectable range of momentum transfer q is $(2.5 < q < 7.5) \text{ nm}^{-1}$ (q is defined here
282 as $q = 4\pi \sin\theta / \lambda$, where θ is the scattering angle and λ the wavelength of the X-

283 rays). Complementary X-ray scattering data were collected at the I911-4 beamline of
284 MAX IV laboratory using a 2D CCD detector (165 mm diameter, from Marresearch,
285 GmbH) and 0.91 Å wavelengths.

286 The samples were mounted in a custom-made sample holder²² which allows
287 temperature control in the range of -30 °C to 45 °C and pressures in the range from
288 ambient to 20 bar. To allow X-rays to pass through the sample, the cell has Kapton
289 windows on both sides of the sample volume. Internal channels connect gas from
290 valves on the surface of the cell to the sample volume, and the gas pressure is
291 controlled by standard reduction valves. The sample cell is depicted in figure S2 in the
292 supporting information.

293 In both X-ray setups, two-dimensional diffractograms were recorded and then
294 azimuthally averaged to produce plots of intensity versus scattering vector, I vs q .
295 Data reduction consisted in subtracting a background and normalizing the intensity
296 profiles to the peak produced by the Kapton windows (see Hemmen et al.²² for
297 details). The intensity, position and width of the intercalation peaks were found by
298 fitting the peaks to Pseudo-Voigt profiles^{54,55}.

299 The LiFh clay mineral used in the experiments was purchased from Corning Inc. (with
300 nominal chemical formula: $M_x(Mg_{6-x}Li_x)Si_8O_{20}F_4$ per unit cell⁵⁶, where M is the
301 interlayer cation (Li^+ , Na^+ and Ni^{2+}) and x the amount which balances the charge of
302 clay mineral layers ($x = 1.2$ for monovalent ions, and $x = 0.6$ for divalent ions). Each
303 sample consisted of 7 ± 1 mg of clay powder packed in the available space in the
304 sample chamber. Typically such packed clay powder samples have a mesoporosity of
305 about 40%⁴⁹, which in the present case enables access of the employed gases to the
306 layered nanoporous structures that make up the individual powder grains.

307 At ambient conditions, these clay mineral samples are in the monohydrated state^{9,57}.
308 Since the uptake of the CO_2 molecules may be affected by the initial H_2O
309 concentration⁵⁸, we investigated dehydrated native samples. For dehydration, the

310 samples were heated in an oven at 125 °C for more than three hours. To remove
311 residual humidity from the cell after loading the clay, and to ensure that the sample
312 remained dry, the cell was flushed with N₂-gas. An X-ray scan was also recorded at
313 ambient temperature and pressure while flushing with N₂ to confirm that the sample
314 remained dehydrated before starting the CO₂ intercalation experiments. The sample
315 was subsequently cooled to -15 °C temperature before the gas was changed to CO₂.
316 The gas outlet of the cell was closed and the pressure increased.

317 The CO₂ used for experiments has a purity of 99.999% (Yara Praxair, grade 5). The
318 N₂ gas has a purity of 99.9999% (Yara Praxair, grade 6). To obtain a satisfactory
319 signal-to-noise ratio, we varied the acquisition times from 30 to 60 minutes,
320 depending on CO₂ pressure, due to differences in X-ray absorption.

321 Pressure-composition-Temperature (pcT) isotherms were measured in a calibrated in-
322 house built (IFE, Kjeller) volumetric Sieverts-type apparatus in order to obtain
323 information on CO₂ adsorption. Approximately 300 mg of Li-fluorohectorite was
324 inserted in a sample holder and was degassed at 115 °C under dynamic vacuum (<10
325 mbar), overnight, to remove residual humidity. Adsorption isotherms were acquired in
326 the 0 – 45 bar range, with 3 bar step between each aliquot measurement at room
327 temperature. The CO₂ adsorption data were baseline corrected by the adsorption data
328 collected from N₂.

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518 Author contribution statement

519 J.O.F and K. D. K. planned the experiments. H.H., K.R. and L.M. designed the sample
520 cell used for the X-ray experiments. L.M., Z.R. and G.J. da S. performed the X-ray
521 experiments at NTNU. H.H., K.R., J.O.F. and T. S. P. performed the synchrotron
522 experiments at Maxlab. P.A.S., G.N.K. and K.D.K. performed the pcT experiments and
523 the associated data analysis. L.M., M.J. and G.J. da S. did the main part of the X-ray

524 data analysis. L.M. and J.O.F. wrote the discussion of the results and also the
525 manuscript, and all authors revised the manuscript before submission.

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